

AMENDMENTS TO THE CLAIMS

1. (currently amended) A process for polymerizing in a first polymerization at least one olefinic monomer selected from ~~the group comprising~~ ethylene, propylene ~~and~~ 1-butene or mixtures thereof in a first loop reactor in the presence of a polymerization catalyst at from 20 to 150°C, but below the melting point of a polymer to be formed, and a pressure of from 5 to 100 bar, where the polymer formed is present in a suspension in a liquid or supercritical suspension medium and wherein the suspension is circulated by means of an axial pump, wherein the loop reactor comprises a cyclic reactor tube whose diameter varies by at least 10%, based on the predominant reactor tube diameter, and in which there is at least one widening and narrowing in a region other than that of the axial pump, wherein an olefin polymer of ethylene, propylene, butene or mixtures thereof is formed.
2. (currently amended) A process for polymerizing in a first polymerization at least one olefinic monomer selected from ethylene, propylene, 1-butene or mixtures thereof in a first loop reactor in the presence of a polymerization catalyst at from 20 to 150°C, but below the melting point of a polymer to be formed, and a pressure of from 5 to 100 bar, where the polymer formed is present in a suspension in a liquid or supercritical suspension medium and wherein the suspension is circulated by means of an axial pump, wherein the loop reactor comprises a cyclic reactor tube whose diameter varies by at least 10%, based on the predominant reactor tube diameter, and in which there is at least one widening and narrowing in a region other than that of the axial pump~~The polymerization process as claimed in claim 1,~~ wherein the polymerization is carried out at an average solids concentration in the reactor of more than 53% by weight, based on the total mass of the contents of the reactor, in the case of continuous product discharge and at an average solids concentration in the reactor of more than 45% by weight, based on the total mass of the contents of the reactor, in the case of discontinuous product discharge.
3. (currently amended) The process as claimed in claim 1, ~~wherein there is~~further comprising a widening and narrowing of the reactor tube in the region of the axial pump.

4. (currently amended) The process as claimed in claim 1, ~~wherein the at least one olefinic monomer comprises ethylene as a first monomer and at least one α -olefin having from 3 to 8 carbon atoms as a comonomer~~further comprising at least one α -olefin having from 3 to 8 carbon atoms as a comonomer, and wherein ethylene is the at least one olefinic monomer.
5. (currently amended) The process as claimed in claim 1, wherein the at least one olefinic monomer is fed in at ~~at least~~ 2 points along the reactor tube.
6. (previously presented) The process as claimed in claim 1, wherein the polymer formed is discharged continuously from the reactor.
7. (previously presented) The process as claimed in claim 1, wherein the polymerization is carried out at an ethylene concentration of at least 10 mol%, based on the suspension medium.
8. (previously presented) The process as claimed in claim 1, wherein the first polymerization in the first loop reactor is preceded or followed by at least one further polymerization step in a second loop reactor or a gas-phase reactor.
9. (previously presented) A loop reactor for the polymerization of olefinic monomers which comprises a cyclic reactor tube and an axial pump for conveying a polymerization mixture, wherein a diameter of the cyclic reactor tube varies by at least 10%, based on a predominant reactor tube diameter, and there is at least one widening and narrowing in a region other than that of the axial pump.
10. (previously presented) The loop reactor as claimed in claim 9, wherein facilities for feeding the monomers into the reactor tube are located at at least 2 points.